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(54) **Polyolefin production**

(57) Use of a metallocene catalyst component of general formula $R''(CpR_m)(Cp'R_n)MQ_2$ in the production of linear low density polyolefin, wherein Cp is a cyclopentadienyl moiety, Cp' is a substituted or unsubstituted fluorenyl ring; R'' is a structural bridge imparting stereorigidity to the component; each R is independently hydrogen or hydrocarbyl having 1 to 20 carbon atoms in which $0 \leq m \leq 4$; each R' is independently hydrocarbyl having 1 to 20 carbon atoms in which $0 \leq n \leq 8$; M is a Group IVB transition metal or vanadium; and each Q is hydrocarbyl having 1 to 20 carbon atoms or halogen; the metallocene having a centroid-M-centroid angle in the range 105° to 125°.

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Description

[0001] The present invention relates to a process for the preparation of polyolefins, especially polyethylenes, the use of metallocene compounds as catalyst components in the production of such polyolefin and the polyolefins obtainable thereby.

[0002] Low density polyethylene (LDPE) offers excellent optical properties and can be processed at relatively low temperatures and pressures while maintaining a good melt strength. LDPE has however limited possibilities for downgauging, due to a low draw ratio, and a low stiffness.

[0003] Linear-low-density polyethylene (LLDPE) has greatly improved downgauging possibilities and excellent tear and impact properties; its stiffness however remains low and its processability is well below that of LDPE. Also, conventional LLDPE's optical properties do not match those of LDPE. Optical properties of LLDPE have been improved by using metallocene-catalysed LDPE (mLLDPE) resins; stiffness is however not improved in these products and the processability of these grades is generally worse than that of conventional LLDPE.

[0004] Wherever high rigidity is needed, LDPE and LLDPE compositions will require overly thick structures. Especially for LLDPE, where excellent impact and tear properties render its downgauging capability useful, the lack of rigidity may be a main drawback. High rigidity maybe a requirement for the end product, it is very often a necessity for product handling.

[0005] In the production of such polyethylene compositions, it is possible to use reaction systems based on a Ziegler-Natta catalyst or a chromium-based catalyst. These reaction systems require a high concentration of comonomer. This suffers from a drawback in that high concentration of comonomer results in increased solubility of the polyethylene produced in a slurry process. One consequence of the increased solubility of polymer is that there is a high incidence of reactor fouling. Use of a high concentration of comonomer is also costly because of the need to recycle unincorporated comonomer.

[0006] It is an aim of the present invention to overcome these disadvantages.

[0007] The present invention provides use of a metallocene catalyst component of general formula $R''(CpR_m)(Cp'R'_n)MQ_2$ in the production of linear low density polyolefin, wherein Cp is a cyclopentadienyl moiety, Cp' is a substituted or unsubstituted fluorenyl ring; R'' is a structural bridge imparting stereorigidity to the component; each R is independently hydrogen or hydrocarbyl having 1 to 20 carbon atoms in which $0 \leq m \leq 4$; each R' is independently hydrocarbyl having 1 to 20 carbon atoms in which $0 \leq n \leq 8$; M is a Group IVB transition metal or vanadium; and each Q is hydrocarbyl having 1 to 20 carbon atoms or halogen; the metallocene having a centroid-M-centroid angle in the range 105° to 125° .

[0008] Figure 1 shows the effect of decreasing the centroid-M-centroid angle in Zr-based metallocenes. The metallocenes of the present invention have a very open structure which permits the facile incorporation of comonomer with larger substituents such as hexene in polyolefin production. In this way, LLDPE with densities around 0.9 or lower may be produced at a commercially acceptable polymerisation temperature in a slurry process. The production of LLDPE with such low densities has hitherto not been possible with Cr-based and closed structure Cent-Zr-Cent ($>125^\circ$) metallocenes in a loop slurry process. Lower comonomer concentrations need be used in the process thereby reducing the likelihood of reactor fouling and avoiding excessive use of expensive comonomer.

[0009] Preferably Cp is a substituent cyclopentadienyl in which each R is independently XR^*3 in which X is C or Si and each R* is independently H or hydrocarbyl having 1 to 20 carbon atoms. More preferably the cyclopentadienyl is substituted with Ph_2CH , Me_3C , Me_3Si , Me, Me and Me_3C , Me and $SiMe_3$, Me and Ph, or Me and $CH_3-CH-CH_3$.

[0010] Preferably, each R' is independently YR'''_3 in which Y is C or Si and each R''' is independently H or hydrocarbyl having 1 to 20 carbon atoms.

[0011] The structural bridge R'' is generally alkylidene having 1 to 20 carbon atoms, a dialkyl germanium or silicon or siloxane, alkyl phosphine or amine, preferably Me-C-Me, Ph-C-Ph, $-CH_2-$, Et-C-Et, Me-Si-Me, Ph-Si-Ph or Et-Si-Et.

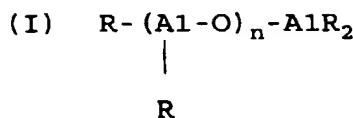
[0012] The metal M is preferably Zr or Hf and each Q is preferably Cl.

[0013] In order to maximise comonomer incorporation, it is preferred that the centroid-M-centroid angle is no more than 119° .

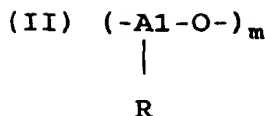
[0014] In a further aspect, the present invention provides a process for the preparation of a linear low-density polyolefin, which comprises reacting an olefin monomer with hydrogen and an α -olefin comonomer in the presence of a catalyst comprising (i) the metallocene catalyst and (ii) an aluminium- or boron-containing cocatalyst. The comonomer is preferably hexene, typically present in an amount of from 2 to 10, preferably 2 to 5% by weight of the total reaction mixture.

[0015] Suitable aluminium-containing cocatalysts comprise an alumoxane, an alkyl aluminium and/or a Lewis acid.

[0016] The alumoxanes usable in the process of the present invention are well known and preferably comprise oligomeric linear and/or cyclic alkyl alumoxanes represented by the formula:



for oligomeric, linear alumoxanes and



for oligomeric, cyclic alumoxane, wherein n is 1-40, preferably 10-20, m is 3-40, preferably 3-20 and R is a C₁-C₈ alkyl group and preferably methyl. Generally, in the preparation of alumoxanes from, for example, aluminium trimethyl and water, a mixture of linear and cyclic compounds is obtained.

[0017] Suitable boron-containing cocatalysts may comprise a triphenylcarbenium boronate such as tetrakis-pentafluorophenylborato-triphenylcarbenium as described in EP-A-0427696, or those of the general formula [L⁺-H]⁺ [B Ar₁ Ar₂ X₃ X₄]⁻ as described in EP-A-0277004 (page 6, line 30 to page 7, line 7).

[0018] The catalyst system may be employed in a solution polymerisation process, which is homogeneous, or a slurry process, which is heterogeneous. In a solution process, typical solvents include hydrocarbons with 4 to 7 carbon atoms such as heptane, toluene or cyclohexane. In a slurry process it is necessary to immobilise the catalyst system on an inert support, particularly a porous solid support such as talc, inorganic oxides and resinous support materials such as polyolefin. Preferably, the support material is an inorganic oxide in its finely divided form.

[0019] Suitable inorganic oxide materials which are desirably employed in accordance with this invention include Group 2a, 3a, 4a or 4b metal oxides such as silica, alumina and mixtures thereof. Other inorganic oxides that may be employed either alone or in combination with the silica, or alumina are magnesia, titania, zirconia, and the like. Other suitable support materials, however, can be employed, for example, finely divided functionalized polyolefins such as finely divided polyethylene.

[0020] Preferably, the support is a silica having a surface area comprised between 200 and 900 m²/g and a pore volume comprised between 0.5 and 4 ml/g.

[0021] The amount of alumoxane and metallocenes usefully employed in the preparation of the solid support catalyst can vary over a wide range. Preferably the aluminium to transition metal mole ratio is in the range between 1:1 and 100:1, preferably in the range 5:1 and 50:1.

[0022] The order of addition of the metallocenes and alumoxane to the support material can vary. In accordance with a preferred embodiment of the present invention alumoxane dissolved in a suitable inert hydrocarbon solvent is added to the support material slurried in the same or other suitable hydrocarbon liquid and thereafter a mixture of the metallocene catalyst component is added to the slurry.

[0023] Preferred solvents include mineral oils and the various hydrocarbons which are liquid at reaction temperature and which do not react with the individual ingredients. Illustrative examples of the useful solvents include the alkanes such as pentane, iso-pentane, hexane, heptane, octane and nonane; cycloalkanes such as cyclopentane and cyclohexane, and aromatics such as benzene, toluene, ethylbenzene and diethylbenzene.

[0024] Preferably the support material is slurried in toluene and the metallocene and alumoxane are dissolved in toluene prior to addition to the support material.

[0025] Where the reaction is performed in a slurry using, for example, isobutane, a reaction temperature in the range 70°C to 110°C may be used. Where the reaction is performed in solution, by selection of a suitable solvent a reaction temperature in the range 150°C to 300°C may be used. The reaction may also be performed in the gas phase using a suitably supported catalyst.

[0026] A linear low-density polyethylene is obtainable from the process with a density below 0.93g/cc and preferably in the range 0.90 to 0.92. The polyethylene preferably has a molecular weight distribution in the range 2 to 4.5, preferably around 3 and more preferably is partially long chain branched so as to facilitate processing.

[0027] This invention will now be described in further detail by way of example only, with reference to the following

Examples and accompanying drawings, in which:

[0028] FIGURE 1 shows centroid-M-centroid angles for some metallocenes.

Example 1

Catalyst Preparation

[0029] $\text{Me}_2\text{CCpFluZrCl}_2$ was prepared in accordance with the method of Razavi and Ferrara published in Journal of Organometallic Chemistry, 435 (1992) pages 299 to 310.

[0030] The support used in a silica having a total pore volume of 4.22 ml/g and a surface area of 322 m²/g. This silica is further prepared by drying in high vacuum on a schlenk line for three hours to remove the physically absorbed water. 5g of this silica are suspended in 50 ml of toluene and placed in a round bottom flask equipped with magnetic stirrer, nitrogen inlet and dropping funnel.

[0031] An amount of 0.31 g of the metallocene is reacted with 25 ml of methylalumoxane (MAO 30 wt% in toluene) at a temperature of 25°C during 10 minutes to give a solution mixture of the corresponding metallocenium cation and the anionic methylalumoxane oligomer.

[0032] Then the resulting solution comprising the metallocenium cation and the anionic methylalumoxane oligomer is added to the support under a nitrogen atmosphere via the dropping funnel which is replaced immediately after with a reflux condenser. The mixture is heated to 110°C for 90 minutes. Then the reaction mixture is cooled down to room temperature, filtered under nitrogen and washed with toluene.

[0033] The catalyst obtained is then washed with pentane and dried under a mild vacuum.

Examples 2 to 7

Bench Scale Polymerisation procedures and results

[0034] Each polymerisation run was performed as described in the following Tables in a 4l autoclave type reactor. In all cases a polymerisation temperature of 80°C was used and the diluent was 2l of isobutane. The catalyst in each case was prepared in accordance with the method indicated.

[0035] It will be apparent from each of Examples 2a, 2b, 2c and 3, as set out in Tables 1 to 4 respectively, that polyethylene products of low density are obtainable according to the invention, especially in the presence of hexene comonomer. High molecular weights are also apparent. This contrasts with comparative Examples 4 to 7 where higher densities are obtained.

Table 1 - Polymerization with $\text{Ph}_2\text{COPh}_2\text{ZrCl}_2/\text{SiO}_2\text{ASAHI}$, H121c.MAO* (Example 2a)

Influence of the hexene/ethylene wt ratio on the fluff density

Entry	C6/C2 wt% ratio	Hourly Prod. (gPE/gcat/h)	MI ₂ (g/10min)	HIMI (g/10min)	SR	Density (g/cc)	Mn (kDa)	Mw (kDa)	Mz (kDa)	D	D'
1	0.00	820	0.06	2.09	37	0.942	43	201	650	4.7	3.2
2	0.41	1,620	too low	0.32	/	0.914	76	304	918	4.0	3.0
3	0.61	2,540	too low	0.17	/	0.918	76	336	958	4.4	2.9
4	0.81	2,130	too low	0.36	/	0.912	81	307	902	3.8	2.9
5(1)	1.22	700	0.06	2.74	44	0.908	35	197	677	5.7	3.4
6(2)	1.22	3854	too low	0.08	/	0.898	/	/	/	/	/
7(2)	1.62	12644	too low	0.12	/	0.896	/	/	/	/	/

Monomer: 6wt% ethylene; (1):4wt%ethylene

Hydrogen: 0.25 Nl

Key: MI₂ = Melt index; Mn = number average molecular weight; Mw = weight average molecular weight; D = Mw/Mn; D' = Mz/Mw; SR = Shear Ratio (HIMI/MI₂)

* made according to the method of Razavi and Atwood J. Organometallic Chem. 459 (1993), 117-123.

Table 2 - Polymerization with $\text{Pb}_2\text{CCpFluZrCl}_2/\text{SiO}_2$ ASAHI', H121c.MAO* (Example 2b)Influence of the hexene/ethylene wt ratio on the fluff density

Entry	Ethylene (wt%)	Hydrogen (NL)	1-hexene (wt%)	C6/C2 wt% ratio	Hourly Prod. (gPE/gCat/h)	MI ₂ (g/10min)	HMI (g/10min)	SR	Density (g/cc)
1	6	0.25	2.44	0.41	1,560	11.29	too high	/	0.923
2	4	0.25	4.88	1.22	880	80.00	too high	/	0.918

* made according to the method of Razavi and Atwood J. Organometallic Chem. 452 (1993), 117-123

Table 3 - Polymerization with $\text{Ph}_2\text{CCpFluZrCl}_2/\text{SiO}_2\text{ASAHI H121c.MAO}^*$ (Example 2c)Influence of the hydrogen content on the melt index

Entry	Hydrogen	Hourly Prod. (gPE/gCat/h)	MI, (g/10min)	HLMI (g/ 10min)	SR	Density (g/cc)	MN (kDa)	MW (kDa)	Mz (kDa)	D	D'
1	0.00	880	too low	too low	0.913	-	-	-	-	-	-
2	0.25	1,620	too low	0.32	0.914	76	304	918	444	3.4	3.0
3	1.00	1,200	0.27	9.91	0.918	39	131	444	444	3.4	3.4

C6/C2 wt ratio:0.41

Key: MI₂ = Melt index; Mn = number average molecular weight; Mw = weight average molecular weight;D = Mw/Mn; D' = Mz/Mw; SR = Shear Ratio (HLMI/MI₂)

*made according to Razavi and Atwood J.Organometallic Chem. 497 (1995), 105-111

Table 4

Polymerization with Me ₂ C(3tBuCp)FluZrCl ₂ /SiO ₂ , ASAHI H121C.MAO* (Example 3)							
Entry	Ethylene (wt%)	hydrogen (NI)	C6/C2 wt% ratio	Hourly Prod. (gPE/gCat/h)	MI ₂ (g/10min)	HLMI (g/10min)	Density (g/cc)
1	6	0.25	0.00	900	too low	too low	0.930
2	6	0.25	0.41*	2,670	too low	0.06	0.917
3	6	0.25	0.41	3,280	too low	0.13	0.920
4	6	0.25	0.61*	2,600	too low	0.03	0.913
5	6	0.25	0.61	3,550	too low	0.01	0.913
6	6	0.25	0.81	2,770	too low	0.16	0.913
7	4	0.25	1.22*	1,550	too low	1.20	0.910
8	3	0.25	1.62*	1,410	too low	1.60	0.907

(*): no prepolymer.

* made according to Razavi and Atwood J.Organometallic Chem. 520 (1996), 115-120

Table 5 - Polymerization with Et(THI)₂ZrCl₂/SiO₂, MAO (Example 4 - Comparative)

Entry	Ethylene (Wt%)	Hydrogen (NL)	1-hexene (wt%)	C5/C2 wt%	Hourly Prod. (gPE/gCat/h)	MI ₂ (g/10min)	HLMI (g/10min)	SR	Density
1	6	0.25	0	0	9,175	too low	0.06	/	0.946
2	6	0.25	2.44	0.41	23,000	0.09	6.89	77	0.933
3	6	0.25	3.66	0.61	14,817	0.04	3.85	89	<0.930

Table 6 - Polymerization with Et(Ind)₂ZrCl₂/SiO₂, MAO (Example 5 - Comparative)

Entry	Ethylene (wt%)	Hydrogen (NL)	1-hexene (wt%)	C6/C2 wt% ratio	Hourly Prod. (gPE/gCat/h)	MI ₂ (g/10min)	HMI (g/10min)	SR	Density (g/cc)
1	6	0.25	0.00	0.00	3,430	0.55	28.2	51	0.951
2	6	0.25	0.61	0.10	6,040	0.87	47.5	55	0.942
3	6	0.25	1.22	0.20	7,700	0.05	5.49	122	0.938
4	6	0.25	2.44	0.41	10,280	0.03	4.49	140	0.932
5	6	0.25	3.66	0.61	10,020	0.27	17.97	67	<0.930
6	6	0.25	4.88	0.81	5,600	1.54	73.93	48	<0.930

Table 7- Polymerization with (nBuCp)₂ZrCl₂/SiO₂. MAO (Example 6 - Comparative)

Entry	Ethylene (wt%)	Hydrogen (NI)	1-hexene (wt%)	C6/C2 wt% ratio	Hourly Prod. (gPE/gCat/h)	MI ₂ (g/10min)	HMI (g/10min)	SR	Density
1	6	0.25	0.00	0.00	4,506	0.58	11.43	20	0.956
2	6	0.25	0.30	0.05	4,400	1.66	28.08	17	0.947
3	6	0.25	1.22	0.20	6,480	1.89	30.60	16	0.944
4	6	0.25	2.44	0.41	7,050	2.05	32.54	16	0.936
5	6	0.25	3.66	0.61	6,800	2.36	37.97	16	0.933
6	6	0.25	4.88	0.81	6,720	2.67	44.72	17	0.930

Table 8 - Polymerization with (iBuCp)₂ZrCl₂/SiO₂. MAO (Example 7 - Comparative)

Entry	Ethylene (wt%)	Hydrogen (NI)	1-hexane (wt%)	C6/C2 wt% ratio	Hourly Prod. (gPE/gcat/h)	MI ₂ (g/10min)	HMI (g/10min)	SR	Density
1	6	0.25	0.00	0.00	7,900	3.07	54.38	18	0.955
2	6	0.25	1.22	0.20	8,840	4.290	69.37	16	0.943
3	6	0.25	2.44	0.41	12,520	4.43	69.80	16	0.938
4	6	0.25	3.66	0.61	10,600	4.71	97.57	21	0.934
5	6	0.25	4.88	0.81	7,200	5.16	86.33	17	0.935

Examples 8 to 11

Pilot Plant Scale Polymerisation procedures and results

- 5 **[0036]** The supported metallocene catalyst of Example 2 was used on a pilot plant scale in the 70 litre loop reactor under the conditions set out in Table 9. Table 9 also shows the results of these pilot plant scale examples, which confirm the earlier bench scale results.

TABLE 9

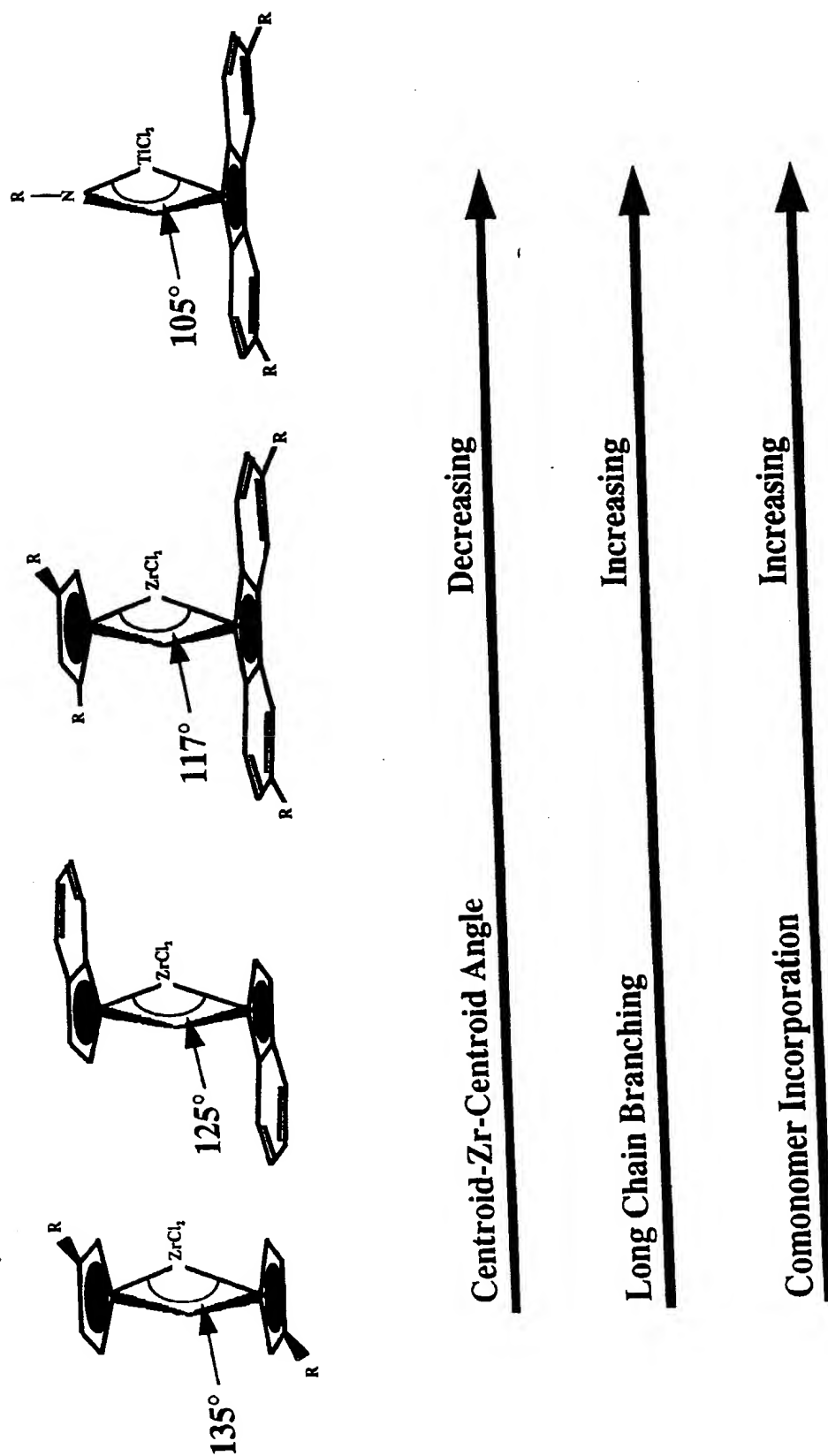
Example	8	9	10	11
CATALYST TYPE	(Ph) ₂ C Cp Flu ZrCl ₂ /SiO ₂ .MAO	(Ph) ₂ C Cp Flu ZrCl ₂ /SiO ₂ .MAO	(Ph) ₂ C Cp ZrCl ₂ /SiO ₂ .MAO	(Ph) ₂ C Cp ZrCl ₂ /SiO ₂ .MAO
LOOP OPER. COND.				
Temp (°C)	85	85	85	80
Alkyl (TIBAL) (ppm/iC ₄)	250	250	250	250
Antifouling (ppm/iC ₄)	4	4	4	4
C ₂ - (kg/h)	7	8.5	7.5	7
C ₆ - (cc/h)	650	1049	1033	1467
H ₂ (NI/h)	5	5	5	5
iC ₄ (kg/h)	26	26	26	86
OFF-GAS FINAL				
2- (wt%)	5.6	6.7	6.0	6.4
C ₆ - (wt%)	0.88	1.38	1.23	2.07
H ₂ (mole%)	0.024	0.028	0.029	0.031
C ₆ -/C ₂ - ratio	0.16	0.21	0.21	0.32
H ₂ /C ₂ - ratio	0.004	0.004	0.005	0.005
CATALYST TYPE	(Ph) ₂ C Cp Flu ZrCl ₂ /SiO ₂ .MAO	(Ph) ₂ C Cp Flu ZrCl ₂ /SiO ₂ .MAO	(Ph) ₂ C Cp Flu ZrCl ₂ /SiO ₂ .MAO	(Ph) ₂ C Cp Flu ZrCl ₂ /SiO ₂ .MAO
FLUFF FINAL				
HLMI (g/10')	0.66	0.53	0.97	1.24
MI ₂ (g/10')	****	****	****	****
MI ₅ (g/10')	****	****	****	****
SR ₂	****	****	****	****
Density (g/cc)	0.918	0.917	0.914	0.912
Bulk Density (g/cc)	0.37	0.37	0.37	0.37

Claims

1. Use of a metallocene catalyst component of general formula $R''(CpR_m)(Cp'R'_n)MQ_2$ in the production of linear low density polyolefin, wherein Cp is a cyclopentadienyl moiety, Cp' is a substituted or unsubstituted fluorenyl ring; R'' is a structural bridge imparting stereoridity to the component; each R is independently hydrogen or hydrocarbyl having 1 to 20 carbon atoms in which $0 \leq m \leq 4$; each R' is independently hydrocarbyl having 1 to 20 carbon atoms in which $0 \leq n \leq 8$; M is a Group IVB transition metal or vanadium; and each Q is hydrocarbyl having 1 to 20 carbon atoms or halogen; the metallocene having a centroid-M-centroid angle in the range 105° to 125°.

2. Use according to claim 1, wherein Cp is a substituted cyclopentadienyl in which each R is independently XR^*_3 in which X is C or Si and each R^* is independently H or hydrocarbyl having 1 to 20 carbon atoms.
3. Use according to claim 2, wherein the cyclopentadienyl is substituted with Ph_2CH , Me_3C , Me_3Si , Me, Me and $\text{Me}_3\text{C,Me}$ and SiMe_3 , Me and Ph, or Me and $\text{CH}_3\text{-CH-CH}_3$.
4. Use according to any one of claims 1 to 3, wherein each R' is independently YR''_3 in which Y is C or Si and each R'' is independently H or hydrocarbyl having 1 to 20 carbon atoms.
5. Use according to any one of the preceding claims, wherein R'' is alkylidene having 1 to 20 carbon atoms, a dialkyl germanium or silicon or siloxane, alkyl phosphine or amine.
6. Use according to claim 5, wherein R'' is Me-C-Me , Ph-C-Ph , $-\text{CH}_2-$, Et-C-Et , Me-Si-Me , Ph-Si-Ph or Et-Si-Et .
7. Use according to any one of the preceding claims, wherein M is Zr or Hf.
8. Use according to any one of the preceding claims, wherein each Q is Cl.
9. Use according to any one of the preceding claims, wherein the centroid-M-centroid angle is no more than 119° .
10. Use according to any one of the preceding claims, wherein the polyolefin is a polyethylene.
11. A process for the preparation of a linear low-density polyolefin, which comprises reacting an olefin monomer with hydrogen and an α -olefin comonomer in the presence of a catalyst comprising (i) a metallocene catalyst component as defined in any one of claims 1 to 10 and (ii) an aluminium- or boron-containing cocatalyst.
12. A process according to claim 11, wherein the olefin monomer is ethylene and the polyolefin is polyethylene.
13. A process according to claim 12, wherein the comonomer comprises 1-hexene.
14. A process according to claim 13, wherein the 1-hexene is present in an amount of from 2 to 10, preferably 2 to 5 % by weight of the total reaction mixture.
15. A process according to any one of claims 11 to 15, wherein the cocatalyst comprises an alumoxane, an alkyl aluminium, a triphenylcarbenium boronate and/or a Lewis acid.
16. A process according to any one of claims 11 to 15, wherein the catalyst is supported on an inert support.
17. A process according to claim 16, wherein the inert support comprises a silica support.
18. A process according to claim 16 or claim 17, which is performed in a slurry..
19. A process according to claim 18, wherein the temperature is from 70°C to 110°C .
20. A process according to any one of claims 11 to 15, which is performed in a solvent at a temperature in the range 150°C to 300°C .
21. A process according to claim 20, wherein the solvent comprises isobutane.
22. A linear low-density polyethylene obtainable from a process according to any one of claims 11 to 18, the density of which is below 0.93 g/cc.
23. A linear low-density polyethylene according to claim 22, wherein the density is in the range 0.90 to 0.92.
24. A linear low-density polyethylene according to claim 22 or claim 23, which has a molecular weight distribution (D) in the range 2 to 4.5.
25. A linear low-density polyethylene according to any one of claims 22 to 24, which is partially long chain branched.

Figure 1





European Patent
Office

EUROPEAN SEARCH REPORT

Application Number
EP 98 11 2233

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int.Cl.6)
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